

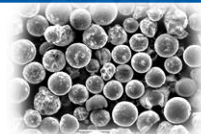
# Adsorption of CO<sub>2</sub> and H<sub>2</sub>O on supported amine sorbents.

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## Objective

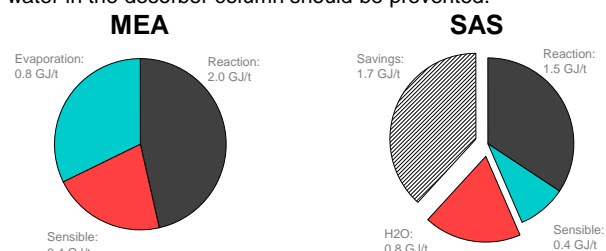
To develop an adsorption based PC capture process with lower capture costs than the MEA based reference process.

A supported amine based process is envisioned to have:

- Lower thermal energy required
- Lower capital investment

## Implications of co-adsorption of H<sub>2</sub>O

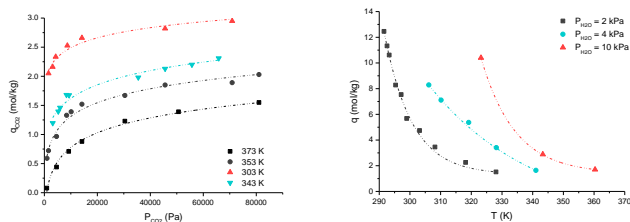
The co-adsorption of water can have a large impact on the process energy demand. Hence the desorption of co-adsorbed water in the desorber column should be prevented.



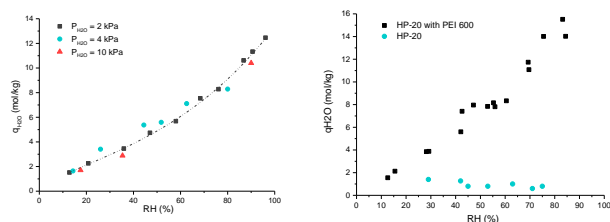
Split-up of heat demand of MEA and SAS process

## Adsorption of H<sub>2</sub>O and CO<sub>2</sub> on supported amine sorbents

Lewatit VP OC 1065 can adsorb much more H<sub>2</sub>O than CO<sub>2</sub>. The highest observed H<sub>2</sub>O capacity is close to the capacity for a filled pore space. CO<sub>2</sub> capacity is limited by the amount of active sites.



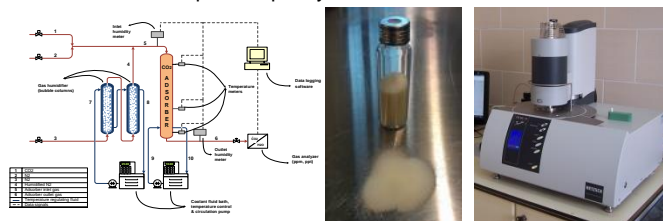
The H<sub>2</sub>O capacity is found to be only a function of RH% which also suggest that condensation is the main adsorption mechanism. Furthermore, H<sub>2</sub>O adsorption measurements were performed for PEI impregnated styrene-divinylbenzene. The H<sub>2</sub>O capacity of the impregnated support material is clearly much high than that of the support only.



Hence, the presence of amine groups causes increased affinity towards the adsorption of H<sub>2</sub>O. This will make it difficult to make a hydrophobic sorbent material with amine functionality.

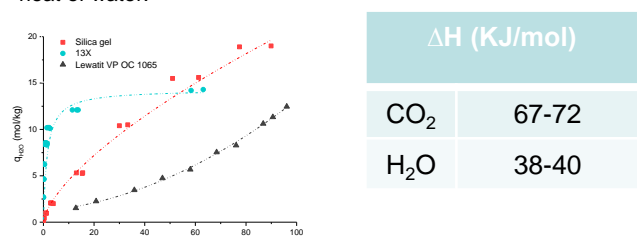
## Experimental

Fixed bed adsorption experiments were combined with TGA analysis. Single component adsorption experiments for both CO<sub>2</sub> and H<sub>2</sub>O were performed as well as co-adsorption of CO<sub>2</sub> and H<sub>2</sub>O to assess differences in adsorption capacity.

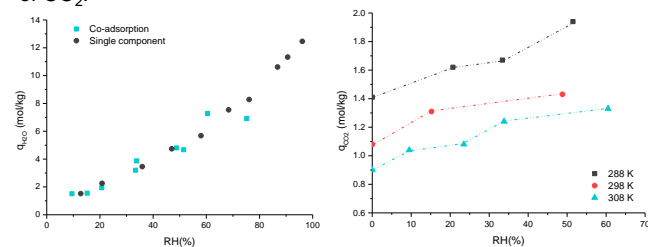


## Adsorption of H<sub>2</sub>O and CO<sub>2</sub> on supported amine sorbents (continued)

The heat of adsorption is much lower for H<sub>2</sub>O than for CO<sub>2</sub>. For water the calculated adsorption heat is close to the evaporation heat of water.



H<sub>2</sub>O does not seem to compete with CO<sub>2</sub> but does interfere in the adsorption process of CO<sub>2</sub> and slightly enhances the CO<sub>2</sub> capacity. The H<sub>2</sub>O is not affected by the simultaneous adsorption of CO<sub>2</sub>.



## Main findings

- The sorbents can adsorb much more H<sub>2</sub>O than CO<sub>2</sub>.
- Adsorption of water is supply limited. Hence, the sorbent will adsorb all incoming water given enough adsorption time.
- The best strategy to prevent the co-adsorption of large quantities of water is to lower the dewpoint of the incoming flue gas. Lowering the dewpoint of the flue gas to 303 K will reduce the energy penalty for water adsorption to 0.2 GJ/t.

## Acknowledgements

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